# Influence of carbon dust in the electrolyte on aluminium electrolysis parameters

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## Abstract



This paper presents the results of the influence of the presence of carbon dust in the electrolyte on cell and electrolyte voltage during aluminium electrolysis. The voltage drop in the cell was determined by the current interruption method. The tests were performed in a laboratory cell with prebaked anodes with varying content of carbon dust added to the electrolyte. The experimental results are indicative of an important relationship between the carbon content in the electrolyte and the cell voltage at constant anode-cathode distance (ACD). The results show that carbon dust in the electrolyte increases electrolyte resistance and consequently electrolyte voltage drop and cell voltage. Despite the fact that carbon is an electrical conductor, carbon particles suspended in the electrolyte under the influence of a DC electric field act as being non-conductive, due to the polarization resistance at the electrolyte/carbon interface.

**Keywords:** Aluminium electrolysis; carbon dust in electrolyte; electrolyte voltage drop; cell voltage.

#### 1. Introduction

In the aluminium industry carbon dust floating in the electrolyte is regarded as a nuisance, and large accumulation of dust is considered to be detrimental to the current efficiency, and it can lead to overheating of the cell [1]. If the amount of dust floating on top of the bath in a cell accumulates, it may then have to be skimmed off. This operation is a very disagreeable job, and the skimming is normally being dumped, representing a loss of bath material. Carbon dust can also accumulate underneath the anodes, apparently increasing the bath resistance [2, 3], causing overheating and possibly uneven current distribution by inhibiting the supply of dissolved alumina to the anode surface. By compensating for the increased resistance, cells with much carbon dust will be operating at a shorter anode-cathode distance, leading to loss in current efficiency.

Anodes are made up of particles of petroleum coke bonded together by a mixture of pitch and fines, forming the so-called binder phase. In the literature it is generally agreed that the cause of carbon dust formation is the fact that the binder coke is more reactive than the aggregate petroleum coke, so that the binder phase is preferentially consumed, and grains of petroleum coke can then be detached, falling into the bath [1].

Carbon dust may also be trapped underneath the anodes, and this dust is regarded as being particularly deleterious, by increasing bath resistance and leading to uneven current distribution. Such accumulation of dust may set up a concentration gradient in the vicinity of the anode with respect to dissolved alumina (risk of anode effect). It may also initiate anode spike formation by inhibiting the normal anode reaction.

Dusting in aluminium reduction cells is one of the visual signs of unwanted anode consumption. Operational irregularities originating from excessive dusting by selective anode oxidation have been experienced by most aluminium plants, particularly in Soderberg cells. Soderberg cells

generate more carbon dust than prebakes, due to the higher pitch content required in soft paste formulation and due to a lower baking temperature.

The amount and behavior of carbon dust depend on several factors, such as: the quality of the anode material, cell design and the operating conditions (the current density, electrolyte composition and electrolyte temperature). Intensive carbon dust formation can be observed prior to or during anode effect, when the carbon is poorly wetted by the electrolyte due to a low alumina concentration. Most of the carbon dust combusts at the surface of the electrolyte, while the remaining part is being skimmed off by the operators. Typically the amount of dust that is being skimmed off can be 20 - 40 kg per tonne Al [4]. However, nowadays the dust problem is more sporadic, but equally damaging for cell performance when it occurs. At reduced interpolar distance or at a particular bath composition, the content of carbon in the electrolyte [5].

The objective of the present work was to measure the voltage drop  $(IR_{el})$  in the electrolyte as a function of different contents of carbon dust in the cryolite melt during laboratory experiments of 6 hours duration.

# 2. Experimental

#### 2.1. Experimental cell

The voltage drop experiments were performed in an air-tight laboratory furnace. Argon (99.999 %) was used as a flushing gas. The cell, shown in detail in Figure 1, consists of a graphite crucible, where the inner wall was covered by a sintered alumina lining. The side of the anode was shielded by a sintered alumina tube, and the top was covered with loose alumina (2 - 3 cm thick layer) in order to prevent any reaction between  $CO_2$  and the carbon anode body. The completely flat anode (made so in order to trap carbon dust underneath the anodes) was 42 mm in diameter and had a threaded hole at the top to connect it to the threaded stainless steel rod (shielded by a sintered alumina tube), which served as the current lead.



Figure 1. The experimental cell.



Figure 7. Uneven anode consumption caused by carbon dust trapped underneath the anode after experiments with 8 wt.% C addition, compared with a new anode.

Accumulation of carbon dust underneath the anode may set up a concentration gradient in the vicinity of the anode with respect to dissolved alumina, and eventually initiate an anode effect. This kind of anode effect was very hard "to kill", and this was the reason for finishing some experiments earlier than after 6 hours.

# 4. Conclusions

- 1. The results of this study are indicative of an important link between the presence of carbon dust in the electrolyte and the cell voltage at constant ACD as well as the voltage drop in the electrolyte.
- 2. The study of current interruption shows that the presence of carbon dust in the electrolyte causes increased voltage drop in the electrolyte.
- 3. The results indicate that accumulation of carbon dust in the electrolyte has a detrimental effect on the behavior (uneven consumption) of the anode and on important parameters of electrolysis, such as cell voltage and ohmic voltage drop in the electrolyte, resulting in increased energy consumption.

# 5. Acknowledgement

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#### 6. References

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